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1   **Method transfer from high-pressure liquid chromatography to ultra-**  
2   **high-pressure liquid chromatography. II. Temperature and pressure**  
3   **effects**

4   Dennis Åsberg<sup>1</sup>, Jörgen Samuelsson<sup>1\*</sup>, Marek Leško<sup>2</sup>, Alberto Cavazzini<sup>3</sup>, Krzysztof  
5   Kaczmarski<sup>2\*</sup> and Torgny Fornstedt<sup>1</sup>

6   <sup>1</sup>Department of Engineering and Chemical Sciences, INTERACT, Karlstad University, SE-651  
7   88 Karlstad, Sweden

8   <sup>2</sup>Department of Chemical and Process Engineering, Rzeszów University of Technology, PL-35  
9   959 Rzeszów, Poland

10   <sup>3</sup>Department of Chemical and Pharmaceutical Sciences, University of Ferrara, IT-44121  
11   Ferrara, Italy

12   \*Corresponding authors' information:

13   J. Samuelsson: Phone: +46 54 700 1620; fax: + 46 73 271 2890; email:  
14   Jorgen.Samuelsson@kau.se.

15   K. Kaczmarski: Phone: +48 17 865 1295; fax: +48 17 854 3655; email:  
16   kkaczmarski@prz.edu.pl.

17   **Abstract**

18   The importance of the generated temperature and pressure gradients in ultra-high-pressure  
19   liquid chromatography (UHPLC) are investigated and compared to high-pressure liquid  
20   chromatography (HPLC). The drug Omeprazole, together with three other model compounds  
21   (with different chemical characteristics, namely uncharged, positively and negatively

22 charged) were used. Calculations of the complete temperature profile in the column at  
23 UHPLC conditions showed, in our experiments, a temperature difference between the inlet  
24 and outlet of 16°C and a difference of 2°C between the column center and the wall. Through  
25 van't Hoff plots, this information was used to single out the decrease in retention factor ( $k$ )  
26 solely due to the temperature gradient. The uncharged solute was least affected by  
27 temperature with a decrease in  $k$  of about 5% while for charged solutes the effect was more  
28 pronounced, with  $k$  decreases up to 14%. A pressure increase of 500 bar gave roughly 5%  
29 increase in  $k$  for the uncharged solute, while omeprazole and the other two charged solutes  
30 gave about 25, 20 and 15% increases in  $k$ , respectively. The stochastic model of  
31 chromatography was applied to estimate the dependence of the average number of  
32 adsorption/desorption events ( $n$ ) and the average time spent by a molecule in the stationary  
33 phase ( $\tau_s$ ) on temperature and pressure on peak shape for the tailing, basic solute.  
34 Increasing the temperature yielded an increase in  $n$  and decrease in  $\tau_s$  which resulted in less  
35 skew at high temperatures. With increasing pressure, the stochastic modelling gave  
36 interesting results for the basic solute showing that the skew of the peak increased with  
37 pressure. The conclusion is that pressure effects are more pronounced for both retention  
38 and peak shape than the temperature effects for the polar or charged compounds in our  
39 study.

40 **Keywords:** Liquid chromatography; Method transfer; UHPLC; Pressure; Temperature;  
41 Stochastic theory.

## 42 **1 Introduction**

43 The interest from the industry to move analytical methods from high-pressure liquid  
44 chromatography (HPLC) to ultra-high-pressure liquid chromatography (UHPLC) has grown in  
45 the last five years [1]. UHPLC provides faster separations and lower solvent consumption

46 compared to HPLC, with preserved column efficiency [2,3]. This is achieved by decreasing  
47 the particle size of the stationary phase and increasing the linear velocity of the mobile  
48 phase. As a consequence, the pressure drop over the column is much larger in UHPLC  
49 compared to HPLC, which leads to significant pressure and temperature (due to viscous  
50 heating and solvent compression) gradients in the column. These gradients have been  
51 shown to affect chromatographic performance and predictability [4].

52 Temperature gradient depends strongly on the method employed to thermostat the column  
53 and has been calculated for different conditions in UHPLC [5–9]. Longitudinal temperature  
54 gradients prevail when the column compartment is close to adiabatic (e.g. in still-air  
55 conditions); they essentially affect only retention time, without compromising column  
56 efficiency. Radial temperature gradients, on the other hand, arise in well-thermostated  
57 conditions (e.g., with waterthermostating), where the center of the column has a different  
58 temperature than the wall. Radial temperature gradients result in decreased column  
59 efficiency and should therefore be avoided.

60 The effect of typical pressures found in UHPLC (ca 1 000 bar) on retention has been  
61 investigated for a number of small compounds and large biomolecules [4,10,11]. For  
62 uncharged species, relatively small changes (of up to 12%) in retention factor were observed  
63 for a pressure increase of 500 bar. For polar or ionic solutes much larger increases, up to  
64 50%, were reported.

65 Stochastic models of chromatography describe the chromatographic processes at a  
66 molecular level [12]. In these models, the chromatographic migration is represented as a  
67 random process in which each molecule, while migrating along the column, performs a  
68 random number of adsorption/desorption steps of random duration. Using the  
69 Characteristic Function formalism in the Fourier domain [13] the stochastic model have been  
70 used for studying heterogeneous adsorption, to including the effect of mobile phase

71 dispersion [14,15], reversed phase [16], chiral [17], size-exclusion [18], and ion-exchange  
72 separations [19].

73 In this study, the pressure effect will be investigated from a stochastic point of view. It has  
74 previously been shown that both efficiency and peak symmetry can decrease with increasing  
75 pressure [20]. Applying the stochastic model at different pressures yield valuable insight in  
76 how the peak shape and retention depend on pressure. This is especially true for  
77 compounds exhibiting heterogeneous adsorption which, to our knowledge, have not been  
78 studied at different pressures. For heterogeneous adsorption, the van't Hoff plot does not  
79 yield any relevant physic-chemical information [21], so by also studying heterogeneous  
80 adsorption at different temperatures using stochastic modelling the effect of pressure and  
81 temperature gradients in UHPLC can be investigated for a heterogeneous adsorption  
82 processes.

83 Additionally, by combining calculations of the temperature profile in the column with the  
84 pressure and temperature dependence of retention factor individual contributions of  
85 pressure and temperature effects can be determined in a more rigorous way than previously  
86 described in the literature.

87 The aim of this study is to investigate the effect of pressure and temperature gradients by  
88 calculating their gradients and determining the individual contributions to retention and  
89 peak shape. Temperature and pressure effects are first investigated separately and then the  
90 combined effect is studied using the same model compounds as in part I [22] (an uncharged,  
91 a positively and a negatively charged and the drug omeprazole). To enable the study of  
92 pressure and temperature effects for compounds with heterogeneous adsorption, stochastic  
93 modelling will be used. Finally we will compare the retention time and efficiency between  
94 HPLC and UHPLC for omeprazole and one degradation product.

95 2 Theory

The stochastic theory [15,23,24] describes the chromatographic process in terms of random variables, namely the time spent by a molecule on the stationary phase (sojourn time) and that elapsed between two successive adsorption/desorption events (flying time). The history of a molecule traveling through a column can be interpreted as the sum of a random number of adsorption/desorption steps performed by that molecule inside the column.

Mathematically, for each molecule, this history will be the convolution integral of the density functions of the time spent on the site. By means of the properties of the Characteristic Function (i.e., the inverse Fourier transform of the probability density function) it is possible to substitute the convolution integral with the product of the elementary characteristic functions and to obtain both the fundamental peak shape parameters (mean, variance, skew, etc.) and the chromatogram itself. In the language of stochastic models, the chromatographic process is a Poisson process, the chromatographic peak being the probability density function of time spent in the column by molecules. Let us define the average number of adsorption/desorption events by  $n$  and the average sojourn and flying times by  $\tau_s$  and  $\tau_m$ , respectively. Under the previous hypotheses, it can be demonstrated that, for a homogeneous surface (that is one characterized by a single sorption site type), the average retention time is given by:

$$t_n = n\tau_{-} + n\tau_{+} \quad (1)$$

114 where  $n\tau_m$  is the time spent, on average, by a molecule in the mobile phase (i.e., the column  
115 hold-up time) and  $n\tau_s$  is the average time a molecule spends in the stationary phase.  
116 For a heterogeneous surface, on the other hand, the corrected retention time will depend  
117 on both the characteristics of the different adsorption sites and their relative abundance on  
118 the phase. In the simple case of a surface paved with only two types of adsorption sites (2-  
119 site heterogeneous model [15]), the average retention time can be expressed as:

$$t_R = n\tau_m + n(\rho_1\tau_{s,1} + \rho_2\tau_{s,2}) \quad (2)$$

121 where  $p_i$  is the relative amount of the  $i$ :th site ( $i = 1, 2$ ) and  $n = n_1 + n_2$ .

122 Through the characteristic function method, the calculation of statistical peak moments is  
123 straightforward [13,15]. Using this statistical moments it is possible to calculate the  
124 parameters traditionally used to describe peak asymmetry, such as peak skew or peak  
125 excess, and to obtain expressions for the height equivalent to a theoretical plate ( $H$ ) or the  
126 number of theoretical plates ( $N$ ). The skew ( $S$ ) for the 1-site and the 2-site models are given  
127 by Eq. 3a and Eq. 3b, respectively [15]:

$$s = \frac{3}{2\sqrt{n}} \quad (3a)$$

$$129 \quad S = \frac{3}{2\sqrt{n}} \frac{p_1 \tau_{s,1}^3 + p_2 \tau_{s,2}^3}{\left( p_1 \tau_{s,1}^2 + p_2 \tau_{s,2}^2 \right)^{3/2}} \quad (3b)$$

130 Column efficiency is determined according to [15]:

$$\frac{1}{N} = \frac{1}{N_D} + \frac{2}{N_M} \left( \frac{k}{k+1} \right)^2 \quad (4)$$

132 where,  $k$  is the retention factor and  $N_D$  is the dispersion effect from the mobile phase  
133 estimated from an unretained marker fitted to the exponentially modified Gaussian  
134 distribution (EMG) and calculated from the distribution's mean and variance.  $N_M$  is defined  
135 for the 1-site model by:

$$N_M = n \quad (5a)$$

137 and for the 2-site model as:

138

$$N_M = n \frac{\left( p_1 + p_2 \left( \tau_{s,2} / \tau_{s,1} \right) \right)^2}{p_1 + p_2 \left( \tau_{s,2} / \tau_{s,1} \right)^2}. \quad (5b)$$

139 To obtain pure data for calculations of adsorption/desorption kinetics, the extra column  
140 contribution to the elution zone must be removed. This was done by fitting the peak of the  
141 void volume marker to an exponentially modified Gaussian distribution and by  
142 deconvolution of the elution peak of the void volume contribution. In this work the  
143 stochastic model parameters were estimated using the super modified sequential simplex  
144 optimization by minimization of the least-squares errors [25]. In this context it is worth  
145 mentioning that the main objective for the stochastic models are to correlate the changes in  
146 peak asymmetry (tailing) with pressure and temperature - not to study band broadening  
147 itself. For the latter, if the band broadening is not tailed so much, general  
148 models/approaches that is sufficient [26].

149 **3 Material and methods**

150 **3.1 Chemicals**

151 The mobile phase was acetonitrile/aqueous-buffer (15 mM phosphate buffer, pH 8.00)  
152 mixtures. Gradient grade acetonitrile was purchased from VWR International (Radnor, PA,  
153 USA). The buffer was prepared from water with conductivity 5.5 µS/m delivered from a Milli-  
154 Q Plus 185 water purification system from Merck Millipore (Billerica, MA, USA) and from  
155 analytical grade sodium phosphate dibasic dihydrate and sodium phosphate monobasic  
156 dihydrate purchased from Sigma-Aldrich (St. Louis, MO, USA). The phosphate buffer was  
157 filtered through a 0.2 µm nylon filter membrane purchased from Whatman (Maidstone, UK)  
158 before it was mixed with acetonitrile. The amount of acetonitrile varied from 7 to 25% v/v,  
159 depending on the solute. Benzyltriethylammonium chloride, BTEAC, (99%), cycloheptanone,  
160 C7, (99%), sodium 2-naphthalenesulfonate, SNS, (≥95%), all from Sigma-Aldrich, and

161 omeprazole sodium monohydrate, OM, (>99%), kindly gifted by AstraZeneca (Mölndal,  
162 Sweden), were used as solutes. BTEAC is positively charged, SNS is negatively charged and  
163 C7 and OM are uncharged at pH 8. The column hold-up volume was determined with sodium  
164 nitrate (≥99.0%) purchased from Sigma-Aldrich.

165 **3.2 Chromatographic equipment**

166 The HPLC system was an Agilent 1200 chromatograph (Agilent Technologies, Palo Alto, CA,  
167 USA) equipped with a binary pump, an auto sampler, a diode-array UV-detector and a  
168 thermostated still air column oven. The extra column volume from the auto sampler to the  
169 detector was 0.037 mL and has been subtracted from the experimental data. The HPLC  
170 column was a 100 × 4.6 mm XBridge BEH C<sub>18</sub> column with an average particle diameter of 3.5  
171 µm and column hold-up volume 0.97 mL. The physicochemical properties of the column are  
172 reported in Table 1. As the column was thermostated in a still air compartment, it can be  
173 assumed that it is under adiabatic conditions [9].

174 The UHPLC system was a Waters Acquity UPLC H-class (Waters Corporation, Milford, MA,  
175 USA) equipped with quaternary pump system, an auto sampler, a diode -array UV-detector  
176 and a thermostated column oven. Also in this case, one may assume the column to be under  
177 adiabatic conditions. The extra column volume from the auto sampler to the detector was  
178 0.027 mL and has been subtracted from the experimental data. The UHPLC column was a 50  
179 × 2.1 mm Acquity UPLC BEH C<sub>18</sub> with an average particle diameter of 1.7 µm. The physico-  
180 chemical properties of the column are given in Table 1. The flow rates of the respective  
181 systems used depended on the goals of the experiments and are mentioned in connection to  
182 the actual experiment, below. As example, for fundamental studies in UHPLC we used a very  
183 low flow rate to avoid pressure and temperature gradients whereas for optimized UHPLC  
184 experiments we used a high flow rate.

185    **3.3 Temperature, mass flow and pressure measurements**

186    The temperature of the column wall was measured by attaching three PT-100 (4-wire)  
187    resistance temperature detectors from Pentronic AB (Gunnebo, Sweden) directly on the  
188    column surface. For the UHPLC column, they were attached on the column wall at 10.7, 21.9  
189    and 35.0 mm from the column inlet and for HPLC they were placed at 21 and 81 mm from  
190    the inlet. A thermal adhesive from Arctic Silver Inc. (Visalia, CA, USA) was used to attach  
191    them. The PT-100 elements had the accuracy  $\pm 0.2^\circ\text{C}$  and were verified in house against a  
192    reference thermometer.

193    The total mass flow was measured by connecting a mini CORI-FLOW Coriolis mass flow  
194    meter after the detector which was purchased from Bronkhorst High-Tech B.V. (Ruurlo,  
195    Netherlands) and had accuracy equal to  $\pm 0.2\%$  of the mass flow.

196    The pressure at the column inlet and outlet was determined by repeating the experiments  
197    first with the capillary going to the column inlet reconnected directly to waste and then with  
198    the column replaced by a zero-volume union. The temperature was measured at the flow  
199    rates 0.25, 0.50, 1.00 and 1.20 mL/min for UHPLC and at 0.40 and 1.00 mL/min for HPLC. The  
200    mobile phase was 25% acetonitrile as this composition corresponds to the largest viscosity  
201    of the mobile phase [27].

202    **3.4 Calculating temperature profiles**

203    The experimentally measured axial temperature difference between column inlet and outlet  
204    was less than  $0.5^\circ\text{C}$  in HPLC at flow rate  $\leq 1 \text{ mL/min}$  and in UHPLC at flow rate  $\leq 0.25$   
205    mL/min. This temperature difference is deemed negligible so these conditions were not  
206    modelled.

207    The modelling of temperature profiles in chromatographic columns was done with the same  
208    method as described in refs. [8,9]. This method combines models of heat and mass transfer

209 and mobile phase velocity distribution. In these calculations, the mass flow measured  
210 externally was used in place of the set up volumetric flow rate. The external heat transfer  
211 coefficient and the parameter in the Blake-Kozeny-Carman correlation were estimated by  
212 minimizing the differences between calculated and experimental values of column outlet  
213 pressure and temperature (measured at the third temperature sensor). The external heat  
214 transfer coefficient was equal to  $30 \text{ W}/(\text{m}^2 \text{ K})$  and the Blake-Kozeny-Carman parameter was  
215 146. At the different flow rates, calculations were validated by comparing the estimated  
216 temperature at the column wall (at the positions of the temperature sensors) with the  
217 experimental temperatures. The agreement between calculated and experimental data was  
218 very satisfactory, with relative errors smaller than 0.5%.

219 **3.5 Chromatographic experiments**

220 Triplicate analytical injections of the four compounds were done at different temperatures  
221 in HPLC and UHPLC and for different pressures for UHPLC. BTEAC (0.01 g/L) was studied at  
222 7% acetonitrile in the eluent, SNS (0.001 g/L) at 15% and C7 (1 g/L) and OM (0.025 g/L) at  
223 25%. The column hold-up volume was measured with  $\text{NaNO}_3$  (0.005 g/L) before each  
224 injection. In HPLC it was equal to 1.00, 0.96 and 0.93 mL and in UHPLC it was 0.11, 0.10, 0.10  
225 mL for 7%, 15% and 25%, respectively. Injection volumes were 5  $\mu\text{L}$  in HPLC and 2  $\mu\text{L}$  in  
226 UHPLC while all compounds were detected at 220 nm except C7, which was detected at 280  
227 nm. The flow rates were 1.00 and 0.13 mL/min in HPLC and UHPLC, respectively, which  
228 resulted in maximum pressure drops of 150 and 100 bar over the columns (negligible  
229 pressure and temperature gradients).

230 When investigating the effect of temperature, the temperature was changed in 5°C  
231 increments and analytical peaks were recorded at each temperature. The interval for HPLC  
232 was 20-40°C and for UHPLC 30-50°C. The intervals were different due to different technical  
233 limitations: the HPLC column thermostat was unable to have stable temperatures >40°C

234 while the UHPLC thermostat could not operate in a reliable way at temperature <25°C. The  
235 pressure was studied by placing a restriction capillary between the column outlet and the  
236 detector. The extra column contributions from the restriction capillaries were measured and  
237 accounted for in the calculations, by lifting out the column and injecting the sample at each  
238 restriction capillary set up. As restriction capillaries LC PEEKsil tubing with inner diameter 25  
239 ± 1 µm from SGE Analytical Science (Milton Keynes, U.K.) was used with lengths 5, 10, 15 and  
240 20 cm. This approach allows to minimize pressure and temperature gradients over the  
241 column. The pressure used in the calculations is taken as the average pressure in the column  
242 when assuming a linear pressure drop over the column [28] and is denoted  $P_{\text{avg}}$ . It is  
243 calculated as:

$$244 \quad P_{\text{avg}} = \frac{P_{\text{col. inlet}} - P_{\text{col. outlet}}}{2} + \Delta P_{\text{after col.}} \quad (6)$$

245 where  $P_{\text{col. inlet}}$  and  $P_{\text{col. outlet}}$  is the pressure at the column inlet and outlet while  $\Delta P_{\text{after col.}}$  is the  
246 total pressure drop from the column outlet to atmosphere including the restriction capillary.  
247 The pressures in Eq. 6 were determined separately for all experimental systems. Five  
248 different pressures were investigated for each solute;  $P_{\text{avg}, 25\%}$  = 53, 174, 302, 420, 550 bar,  
249  $P_{\text{avg}, 15\%}$  = 53, 175, 314, 419, 552 bar and  $P_{\text{avg}, 7\%}$  = 51, 167, 301, 398, 524 bar, where the "%" denotes the fraction of acetonitrile in the mobile phase.

## 251 4 Results and discussion

252 To demonstrate that a direct method transfer from HPLC to UHPLC is not always  
253 straightforward, the four compounds employed in this work have been eluted on the two  
254 columns under isocratic conditions and typical flow rates of HPLC and UHPLC (1.0 and 1.2  
255 ml/min, respectively). It is worth to mention that these flow rates were not obtained as the  
256 optimal flow rate in a van Deemter curve, as the study of column efficiency was not the

257 purpose of this work. Temperature in both cases was set to 40°C. Overlaid chromatograms  
258 are presented in Fig. 1 where, for the sake of comparison, retention is expressed as column  
259 volumes instead of retention time. It is evident from Fig. 1 that the retention in column  
260 volumes is longer for UHPLC (gray lines) compared to HPLC (black lines), especially for the  
261 late eluting peaks which also exhibit more tailing in UHPLC. This difference in retention  
262 might be caused by factors such as different pressures, temperature gradients and column  
263 chemistry. From calculating the efficiency with the moment method for HPLC and UHPLC in  
264 Fig. 1, it could be seen that, in this case, HPLC condition yielded the highest efficiency. The  
265 average efficiency of three injections were for HPLC 6230, 9430, 10730 and 9330 and for  
266 UHPLC 1610, 3560, 5050 and 4330 for BTEAC, SNS, C7 and OM, respectively. Reasons for the  
267 lower efficiency in UHPLC are most likely that the HPLC column was twice as long as the  
268 UHPLC one, the column loading was higher in the UHPLC experiments and that the extra-  
269 column volume in the UHPLC system was a larger fraction of the column volume.  
270 Temperature gradients causing a radial thermal heterogeneity and pressure gradients could  
271 also affect the efficiency.

272 Through the aid of the stochastic modelling and by  $\ln(k)$  vs.  $1/T$  and  $\ln(k)$  vs.  $P$  plots we will  
273 try to investigate the individual contributions of temperature and pressure to retention and  
274 peak shape.

## 275 **4.1 Temperature and pressure effects on retention**

### 276 **4.1.1 Pressure dependence**

277 The slope of  $\ln(k)$  vs.  $P_{\text{avg}}$  plots is equal to  $\Delta V_m = V_{\text{stat.}} - V_{\text{mob.}}$ , i.e. the change in solute molar  
278 volume associated with the transition between the stationary and mobile phase [29].  
279 Generally the solute molar volume is larger in the mobile phase, i.e.  $\Delta V_m < 0$ . According to Le  
280 Chatelier principle, when the pressure is increased the equilibrium between solute

281 molecules in the mobile and stationary phase will be pushed toward the stationary phase ,  
282 resulting in increasing retention time [29,30].

283 The logarithm of the retention factor for different pressures was fitted with linear regression  
284 and the result is presented in Fig. 2. The relationship between  $\ln(k)$  and  $P_{\text{avg}}$  is linear with a  $R^2$   
285 value larger than 0.980. Calculated  $\Delta V_m$  values were  $-11.9 \pm 1.0 \text{ cm}^3/\text{mol}$  for BTEAC,  $-15.5 \pm$   
286  $0.3 \text{ cm}^3/\text{mol}$  for SNS,  $-3.4 \pm 0.3 \text{ cm}^3/\text{mol}$  for C7 and  $-18.4 \pm 0.5 \text{ cm}^3/\text{mol}$  for OM given with a  
287 95% confidence interval. These observations are in good agreement with those reported by  
288 Fallas et al. [10,11] for a similar system. The negative  $\Delta V_m$  is attributed to the partial loss of  
289 the solvation layer of the solutes when they move from the mobile to the hydrophobic  
290 stationary phase. The difference in  $\Delta V_m$  between uncharged and ionized solutes is believed  
291 to be due to the hydration of the ions which are partially lost when entering the stationary  
292 phase. However, this clearly shows that pressure is a factor that needs to be considered  
293 because it could affect the selectivity as well as retention.

294 **4.1.2 Temperature dependence**

295 To better understand the effect of viscous heating, the temperature gradients in the column  
296 were quantified. The 2-dimensional temperature profile corresponding to UHPLC conditions  
297 of 25% acetonitrile and flow rate 1.2 mL/min (same as Fig. 1) has been calculated and shown  
298 in Fig. 3. The dotted line at 1.05 mm represents the inner column wall. Because the column  
299 temperature profile was assumed to be radially symmetrical, only half of the temperature  
300 contour plot is shown. As can be seen from Fig. 3, the temperature along the column, i.e.  
301 longitudinally, increased  $\approx 16^\circ\text{C}$  from the inlet to the outlet and the temperature inside the  
302 column from centrum to wall, i.e. radially, decreased  $\approx 2^\circ\text{C}$  at most. The values calculated for  
303 this specific system are close to those reported in the literature [6,9] for similar pressure  
304 drops over the column.

305 The effect of the temperature gradient on retention was estimated by calculating the local  
306 propagation speeds along the column by first calculating the geometric radial average  
307 temperature using the temperature profile in Fig. 3. Then the temperature dependence of  
308 the retention factor was determined by fitting the logarithm of retention factors to the  
309 reciprocal temperature, Fig. 4. Linearity of  $\ln(k)$  vs.  $1/T$  was observed in all cases with  $R^2$ -  
310 values above 0.990, except for BTEAC for which a slight nonlinearity was observed with  $R^2$ -  
311 value 0.960. The retention factor of all solutes decreases with temperature, which is the  
312 common behavior in RP-LC for moderate temperature variations. Combining this  
313 information the retention time was estimated by integrating the solute local propagation  
314 speed along the UHPLC column. The uncharged solute, C7, is least affected by the  
315 temperature gradient with a decrease in  $k$  of roughly 5%. The positively charged solute,  
316 BTEAC, is somewhat more sensitive and  $k$  decreases about 10% while the negatively charged  
317 solute, SNS, is most affected by temperature and  $k$  decreases almost 14%. The retention  
318 factor of OM decreases approximately 9%, which places it in the same region as the other  
319 two charged solutes.

320 **4.1.3 The relative importance of temperature and pressure gradients**

321 In an attempt to compare the relative importance of pressure and temperature on retention  
322 in UHPLC, the results from Sec. 4.1.1 and 4.1.2 have been combined in Fig. 5, where the  
323 retention factors of the four investigated molecules have been normalized against the  
324 respective retention factor at 0.13 mL/min (where pressure and temperature gradients are  
325 negligible). In Fig. 5, white bars show the estimated contribution for temperature, while gray  
326 bars show the pressure contribution, which has been estimated by assuming a linear  
327 pressure gradient over the column. Finally, black bars represent the observed, experimental  
328 retention factors found in UHPLC.

329 The pressure and temperature have opposite effects on retention and will therefore, to a  
330 certain degree, cancel each other. Under typical UHPLC conditions, the pressure effect is  
331 always larger than the temperature effect, except for C7. For C7, which is uncharged, the  
332 pressure effect is very small. Both the pressure and temperature effects are solute  
333 dependent. In particular, our data show that charged solutes and those with larger  
334 molecular weight are most affected by pressure. These results also suggest that in the  
335 method transfer from HPLC to UHPLC, especially if charged solutes are considered, the effect  
336 of the pressure gradient along the column more than that of temperature gradient should  
337 be taken into account, as it is the dominating one.

338 **4.2 Stochastic Modelling**

339 The adsorption isotherms for the modeling compounds has previously been investigated and  
340 it was found that C7 and OM exhibited homogeneous adsorption while SNS and BTEAC had  
341 heterogeneous adsorption [22]. Since the peak shape was also very symmetrical for C7, OM  
342 and SNS, they were described by 1-site stochastic models. One must stress that  
343 heterogeneous adsorption not necessarily results in measurable heterogeneous kinetics.  
  
344 For very symmetrical peak shapes as those observed under our conditions, the number of  
345 adsorption/desorption events ( $n$ ) and adsorption sojourn time ( $\tau_s$ ) are strictly correlated, so  
346 that nonlinear fitting cannot differentiate between them. Therefore, any trends with  
347 temperature or pressure seen for this kind of peaks may be an artifact of nonlinear fitting.  
348 As a consequence, only the range of these parameters is given here. The conclusion is that  
349 for solutes with very symmetrical peaks, the stochastic approach is unable to single out  
350 pressure and temperature effects.  
  
351 For BTEAC, the elution peaks are asymmetrical so the nonlinear fitting could differentiate  
352 between contributions of  $n$  and  $\tau_s$ .

353    **4.2.1 Temperature dependence**

354    For OM, C7 and SNS (1-site model)  $n$  is similar for all three solutes (10 000 to 20 000) in HPLC  
355    and UHPLC with the values for UHPLC being slightly lower.  $\tau_s$  is between 10 and 20 ms and  
356    the values are slightly higher for UHPLC than for HPLC. These observations reflect the fact  
357    that the measured column efficiency is higher in HPLC.

358    BTEAC adsorption is described by a 2-site adsorption isotherm [22] and the elution peaks are  
359    tailing so the 2-site stochastic model has been employed to fit the chromatograms. Site-1 is  
360    where the majority of all adsorption/desorption events take place and the sojourn time for  
361    these sites are in the millisecond scale, Fig. 6. On the other hand, at site-2 only a few  
362    adsorption/desorption events take place. However, the sojourn time found on these sites is  
363    roughly one thousand times longer than on site-1. We observe that the average number of  
364    adsorption/desorption events increases with increasing temperature and that the sojourn  
365    time decreases with increases temperature for both sites and systems. From a fundamental  
366    perspective, increasing the temperature will result in an increased diffusion coefficient both  
367    due to the temperature itself but also due to a reduction in viscosity, as described by the  
368    Stokes–Einstein equation. The faster kinetics will result in increased  $n$  and decreased  $\tau_s$  as  
369    observed. The scatter of the data points in Fig. 6, especially for  $n_1$  and  $n_2$ , is most likely due  
370    to a combination of numerical errors in the optimization and experimental errors.

371    The skew can be seen as a measure of the peak symmetry where a large positive skew  
372    means that the peak is tailing and a negative skew means that the peak is fronting. In this  
373    case the skew decreases with temperature for both HPLC and UHPLC, Fig. 6f, which indicates  
374    that the peak shape becomes more symmetrical when the temperature is increased.  
375    Relating the observation of decreasing skew to Eq. 3b, it is due to the increase in  $n_2$  and the  
376    decrease in  $\tau_{s,2}$  for the slow site with increasing temperature. This also clearly shows that the  
377    tailing observed for BTEAC (see Fig. 1) is due to heterogeneous kinetics.

378    **4.2.2 Pressure dependence**

379    For C7, OM and SNS, that is the compounds described by 1-site stochastic model,  $n$  has been  
380    found to be nearly constant while  $\tau_s$  increase slightly with increasing pressure. In particular,  
381     $n$  was between 8000 and 14000 and  $\tau_s$  between 10 and 22 ms. It has previously been  
382    reported that increasing pressure could result in decreasing efficiency [20]. One probable  
383    explanation to this could be that the viscosity increases with the pressure [31] and as a  
384    result through the Stokes–Einstein equation this will result in an increased diffusion  
385    coefficient. From the stochastic model perspective this will result in reduction in  $n$  because  
386    slower diffusion results in fewer adsorption/desorption events take place. The sojourn time  
387    ( $\tau_s$ ) will increase because it takes longer time for the solute to diffuse out from the stationary  
388    phase. In this study for C7, OM and SNS we observed an increasing sojourn time but more  
389    or less no effect on  $n$ .

390    The results for BTEAC are presented in Fig. 7 and show that on the “fast” adsorption site  
391    there is an increase of  $n_1$  and a decrease in  $\tau_{s,1}$ . While the “slow”, second site, presents a  
392    nearly 50% increase in  $\tau_{s,2}$  with a 500 bar pressure increase. As a consequence, the peak  
393    skew is increased, Fig. 7f and efficiency decrease when the pressure is increased, Fig. 7e.  
394    This increase in peak skew is due to the fact that the solute molecules spend on average a  
395    longer time adsorbed on the slow, second site when the pressure increases which makes the  
396    tailing more pronounced. To understand heterogeneous kinetics pressure dependency  
397    better it should be necessary to include more experiments with focus on several different  
398    kinds of basic compounds, however this is outside the scope of the study. So the presented  
399    result should be viewed as a first observation.

400    From Fig. 6 and Fig. 7, one may conclude that high temperature and low pressure improve  
401    peak shape for BTEAC. We believe that, even though more information must be gathered to  
402    draw any general conclusions, this is an interesting finding.

403    **4.3 Practical implications**

404    To compare the performance of HPLC and UHPLC, retention time, column efficiency and  
405    resolution for a degraded omeprazole sample containing the degradation product H168/66  
406    in small amounts were investigated. The same mobile phase, temperature and stationary  
407    phase chemistry were used. The column dimensions and particle diameters differed; the  
408    HPLC column was 100 × 4.6 mm, 3.5 µm and the UHPLC column was 50 × 2.1 mm, 1.7 µm.  
409    The flow rate and injection volume for HPLC was 2.0 mL/min and 10 µL and for UHPLC they  
410    were scaled according to ref. [32] which yielded 0.86 mL/min and 1 µL. The scaling was done  
411    to keep the reduced linear velocity of the mobile phase constant. At these flow rates the  
412    pressure drop over the HPLC column was 165 bar and 570 bar over the UHPLC column.

413    The chromatograms are presented in Fig. 8, where the retention time for omeprazole is 3.6  
414    longer in HPLC. The retention times, efficiencies (moment method) and resolution factors  
415    (half-height) are presented in Table 2. The efficiency of omeprazole was 29% higher in HPLC  
416    and efficiency for H168/66 was 13% higher, which resulted in a resolution factor that was  
417    about 9% higher in HPLC. However, the loss in efficiency and resolution when switching to  
418    UHPLC are very minor compared to the reduction in run time and resulting decrease in  
419    solvent consumption which makes UHPLC the primary choice in this case. The individual  
420    effects of pressure and temperature gradients in UHPLC are not directly observable since  
421    their effects are convoluted when comparing the different modes in this way.

422    **5. Conclusions**

423    The aim of this study has been to investigate how pressure and temperature affect retention  
424    and peak shape of the solutes in HPLC and UHPLC. To this end, the chromatographic  
425    behavior of four model compounds with different physicochemical properties has been  
426    modeled from both a thermodynamic and a kinetic (microscopic-stochastic) viewpoint. The

427 thermodynamic models showed that the difference in solute molar volume for adsorbed and  
428 in bulk solution, which determines the pressure dependence of the retention factor, was  
429 largest for the polar solute omeprazole which also had the largest molecular weight. When  
430 combining the calculated temperature gradient and the linear pressure gradient the  
431 individual contributions on retention could be determined. The effect of the pressure  
432 gradient was found to be the dominating one and should therefore be taken into account  
433 when switching from HPLC to UHPLC.

434 From the stochastic modelling of the tailing, basic solute it was evident that an increase in  
435 temperature yielded an increase in average number of adsorption/desorption events while  
436 the average time spent by a molecule in the stationary phase was slightly decreasing. For  
437 increased pressure the effect was the opposite. Therefore a high temperature and a low  
438 pressure yielded low tailing. Even though from different perspectives, the conclusions of  
439 these models converge in showing that the effect of pressure gradient along the column is  
440 as important as that of viscous heating. With charged and polar compounds, we found that  
441 the impact of the pressure gradient is even more important than that of viscous heating in  
442 UHPLC for the investigated experimental conditions.

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538 **Figure captions**

539 **Fig. 1:** Overlaid chromatograms for HPLC (black) and UHPLC (gray). All extra-column volumes  
540 have been corrected for and the retention volumes have been normalized with the HPLC and  
541 UHPLC column volumes, respectively. The column temperature was set to 40°C and the

542 pressure drop over the column in HPLC was 100 bar and in UHPLC 800 bar, respectively. This  
543 corresponded to a flow rate of 1.0 mL/min for HPLC and 1.2 mL/min for UHPLC.

544 **Fig. 2:** Experimental retention factors for BTEAC (circles), C7 (squares), SNS (diamonds), and  
545 OM (triangles) for different pressures. Mobile phase compositions were 7, 15 and 25%  
546 acetonitrile for BTEAC, SNS and C7/OM, respectively and flow rate was 0.13 mL/min.

547 **Fig. 3:** Calculated temperature profile in UHPLC for the mobile phase 25/75, v/v  
548 acetonitrile/phosphate buffer at flow rate 1.2 mL/min. The dotted line represents the inner  
549 column wall. At 50 mm the center of the column is warmest (55°C) and the column wall is at  
550 ca 52°C; radius 0 is the center of the column. The pressure over the column is 782 bar.

551 **Fig. 4:** Experimental retention factors for BTEAC (circles), C7 (squares), SNS (diamonds), and  
552 OM (triangles) for different temperatures. Mobile phase compositions were 7, 15 and 25%  
553 acetonitrile for BTEAC, SNS and C7/OM, respectively and flow rate was 0.13 mL/min.

554 **Fig. 5:** The retention factor is compared for four different cases in UHPLC. The baseline is  
555 taken as the retention factor at low flow rate 0.13 mL/min where pressure and temperature  
556 gradients are negligible; the bars denoted “only  $T$ ” represent the effect caused only by the  
557 temperature gradient; “only  $P$ ” denotes the case with only the pressure effect present and  
558 “observed” represents actual experimental result where both pressure and temperature  
559 effects are present.

560 **Fig. 6:** Stochastic modelling of BTEAC which is described by a 2-site model at different  
561 temperatures.  $N$  is the column efficiency determined with Eq. 4 and  $S$  is the skew  
562 determined with Eq. 3b.

563 **Fig. 7:** Stochastic modelling of BTEAC which is described by a 2-site model at different  
564 pressures.  $N$  is the column efficiency determined with Eq. 4 and  $S$  is the skew determined  
565 with Eq. 3b.

566 **Fig. 8:** Chromatogram from HPLC and UHPLC for omeprazole (large peak) and the  
567 degradation product H168/66 (small peak) for identical mobile phase, stationary phase and  
568 column temperature. Flow rates are 2 mL/min in HPLC and 0.86 mL/min in UHPLC.

**Table 1:**  
Physicochemical properties from the manufacturer of the columns

Property	XBridge BEH-C <sub>18</sub>	AQUITY BEH-C <sub>18</sub>
Average particle size [μm]	3.5	1.7
Pore volume [cm <sup>3</sup> /g]	0.71	0.70
Surface area [m <sup>2</sup> /g]	184	179
Average pore diameter [Å]	138	141
Total carbon content [%]	17.88	17.40
Surface concentration [μmol/m <sup>2</sup> ]	3.36	3.07

**Table 4:** Parameters for the separation of omeprazole and the degradation product H168/66 using HPLC and UHPLC columns, respectively.  $t_r$  is the retention time,  $N$  the efficiency and  $R_s$  the resolution factor.

Solute	Parameter	HPLC	UHPLC
OM	$t_r$ [min]	2.61	0.72
H168/66	$t_r$ [min]	1.74	0.45
OM	$N$	5970	4230
H168/66	$N$	6240	5460
-	$R_s$	9.87	8.99















